

© The Author(s), 2020, published on behalf of Materials Research Society by Cambridge University Press. This is an Open Access article, distributed under the terms of the Creative Commons Attribution licence (http://creativecommons. org/licenses/by/4.0/), which permits unrestricted re-use, distribution, and reproduction in any medium, provided the original work is properly cited.

REVIEW

Renewable hydrogen for the chemical industry

Nigel Rambhujun, Muhammad Saad Salman, Ting Wang, Chulaluck Pratthana, Prabal Sapkota, Mehdi Costalin, Qiwen Lai, and Kondo-Francois Aguey-Zinsou, MERLin, School of Chemical Engineering, The University of New South Wales, Sydney, NSW 2052, Australia

Address all correspondence to Kondo-Francois Aguey-Zinsou at f.aguey@unsw.edu.au

(Received 19 June 2020; accepted 18 August 2020)

ABSTRACT

Hydrogen is often touted as the fuel of the future, but hydrogen is already an important feedstock for the chemical industry. This review highlights current means for hydrogen production and use, and the importance of progressing R&D along key technologies and policies to drive a cost reduction in renewable hydrogen production and enable the transition of chemical manufacturing toward green hydrogen as a feedstock and fuel.

The chemical industry is at the core of what is considered a modern economy. It provides commodities and important materials, e.g., fertilizers, synthetic textiles, and drug precursors, supporting economies and more broadly our needs. The chemical sector is to become the major driver for oil production by 2030 as it entirely relies on sufficient oil supply. In this respect, renewable hydrogen has an important role to play beyond its use in the transport sector. Hydrogen not only has three times the energy density of natural gas and using hydrogen as a fuel could help decarbonize the entire chemical manufacturing, but also the use of green hydrogen as an essential reactant at the basis of many chemical products could facilitate the convergence toward virtuous circles. Enabling the production of green hydrogen at cost could not only enable new opportunities but also strengthen economies through a localized production and use of hydrogen. Herein, existing technologies for the production of renewable hydrogen including biomass and water electrolysis, and methods for the effective storage of hydrogen are reviewed with an emphasis on the need for mitigation strategies to enable such a transition.

Key words: chemical synthesis; circular economy; energy generation; energy storage; environment; environmentally protective; sustainability

Introduction

Hydrogen in the chemical industry

Hydrogen (H_2) is an important component of the universe with an enormous extent of applications. However, it does not

DISCUSSION POINTS

- Hydrogen is already an important feedstock supporting the chemical industry, and this makes the transition away from fossil fuels challenging.
- Green hydrogen could help decarbonize the chemical industry and beyond transform the industry toward "green" products manufacturing.
- What is the current status, and which technologies could support such a transition? What is the role of policy in this?

exist in free form in nature, but rather is bonded inside ubiquitous compounds such as water and hydrocarbons. As a key building block in chemical processes, a huge fraction of current hydrogen production is used in industrial processes such as the synthesis of ammonia and petrochemicals. The global demand for hydrogen, which has tripled since 1975, is growing every year with no signs of slowing down (Fig. 1). As of 2018, the worldwide annual hydrogen production is estimated to be ~74 Mt, with up to ~96% used in the chemical industry, ~42% alone for ammonia production, and ~52% in different refineries.¹ The remaining hydrogen (~6%) is used in other sectors such as glass production and reduction of iron ores (Figs. 1 and 2).

In the chemical industry, ammonia is globally produced through the well-known Haber-Bosch process, in which hydrogen and atmospheric nitrogen are passed over a catalyst at elevated temperatures and pressures. Ammonia is used extensively in agriculture, explosives, and cleaning streams.



Figure 1. Global demand of pure hydrogen in refinery, ammonia, and other sectors for the period 1975–2018. Source: IEA. All rights reserved.¹

Common nitrogen-rich fertilizers including urea and ammonium nitrate are produced directly from ammonia. Urea is obtained after reacting ammonia with CO_2 originating from the steam reforming, while ammonium nitrate is produced through the catalytic oxidation of ammonia with nitric acid. As a carbon-free commodity, ammonia has been touted as a promising alternative to conventional hydrogen storage systems.² However, most of the hydrogen for its production comes from fossil fuels through reforming – which collectively accounts for 830 Mt CO_2 /yr globally.^{1,3} The chemical industry, with 10% of the global energy consumption and 7% of the greenhouse gas emissions,⁴ is also the largest user of energy in the industry sector. Enabling the use of renewable hydrogen could thus have a significant impact in decarbonizing the industry sector. Renewables for green hydrogen production include solar and wind coupled with water electrolysis, solar-thermal, and in a distant future direct photochemical hydrogen generation. However, at the moment, the amount of renewable hydrogen is far from meeting the global needs for hydrogen (Fig. 2).

In the refinery sector, which is one of the biggest consumers, hydrogen is used in upgrading the hydrocarbons. Hydrogen is used to remove sulfur, halides, oxygen, metals, and/or nitrogen impurities, and cracking of heavier to lightweight hydrocarbons to produce many value-added chemicals. Most of these processes need careful conditions with suitable catalysts, which dictate the efficiency of the process.

Many chemical industries also use hydrogen extensively to reduce the degree of unsaturation, taste, and/or odor in fats and oils via a hydrogenation process carried out in the presence of nickel catalysts.^{5,6} This process increases the melting point and enhances the resistance to oxidation with prolonged preservation. In the hydrogenation process, the amount of hydrogen consumed depends on the oil and the degree of hardness (measured by the reduction in iodine number – that is the amount of hydrogen gas equivalent to iodine absorbed), the purity of hydrogen, and the equipment. Assuming that high-quality hydrogen is used, the actual amount of gas required is often ~110% higher than the theoretical values.⁷

The hydrogenation of fats produces trans fats, which have adverse health effects,⁸ but recently, new chemistry has revealed that the formation of trans fats could be avoided by carefully manipulating the selectivity of the catalysts.⁹ It is expected that such selective catalytic hydrogenation processes will be further developed in the future and could help to lower the pernicious effects of saturated fats.¹⁰





At the moment, for all of the mentioned applications, most of the hydrogen is obtained through steam reforming of fossil fuels. In steam reforming, hydrocarbons are converted to carbon monoxide (CO) and H₂, commonly known as synthesis gas or syngas, using steam at high temperature (700-1000 ° C). ¹¹

$$CH_4 + H_2O \leftrightarrow CO + H_2$$
 (1)

However, if hydrogen is to become the fuel of the future, extensive development in advanced technologies for the production of green hydrogen and enabling energy policies are essential to shift our dependence from fossil fuels toward renewables and sustainable hydrogen.

Technologies for renewable hydrogen production

Hydrogen is often described as a clean and sustainable energy vector but in order to live up to this description, renewable methods using sustainable sources need to be the backbone of hydrogen production.¹² In this section, renewable methods to produce H₂ from water and biomass, along with their associated costs – in USD across the manuscript (Fig. 3), are reviewed in comparison to the production cost of hydrogen from steam methane reforming (1.9-2.6 \$/kg H₂) and the 2020 U.S. Department of Energy (DOE) target (2 \$/kg H₂).^{13,14}

For a more in-depth analysis, El-Emam and Ozcan published a comprehensive review on the technological, economic, and environmental aspects of renewable hydrogen production.¹⁵

Making hydrogen from biomass

Biomass currently covers 14% of the total primary energy consumption¹⁶ due to its abundance and ease of accessibility across many countries.¹⁷ Nowadays, as a CO₂ neutral precursor, biomass is considered as an important renewable resource for hydrogen production,¹⁸ although the carbon foot print associated with the use of biomass for hydrogen production may not be neutral. For example, 8.99×10^{-2} CO₂ eqv. g/s is emitted to produce 0.484 MJ/s H₂ from an annual consumption of 2.53×10^{6} kg of biomass.¹⁹ The use of biomass for energy production is often a great concern with respect to land use. However, alternatives likes lignocellulosic waste and crops waste have the potential to address this issue to some extent.²⁰ Other types of "low cost" biomass to produce hydrogen include bio-waste, biogas, industrial organic waste, sewage sludge, biooil, and biochar;²¹⁻²³ and the usual hydrogen content in biomass is \sim 5-7 wt%.²⁴

Currently, the two main routes to produce hydrogen from biomass are through the thermochemical and biochemical process (Fig. 4).^{25,26} Thermochemical processes include pyrolysis, gasification, steam reforming, and supercritical gasification,²¹ whereas biochemical processes include bio-photolysis, biofermentation, and dark fermentation.²⁷ In the biochemical route, biomass can be converted into biofuels through various processes including anaerobic or aerobic digestion, fermentation, and acid hydrolysis.²⁸ Recently, emerging technologies like bio-electrochemical systems have also been used to convert waste treatment into energy production. In this method,







Figure 4. Hydrogen production by different methods from various types of biomass.

electrochemically active micro-organisms (e.g., *Shewanella* oneidensis and *Geobacter sulfurreducens*) are grown under electrochemical interactions with electrodes^{29,30} to catalyze and oxidize organic matter to generate CO₂, electrons, and protons.³⁰ The electrons are transferred to the anode, while the protons move through a membrane to the cathode, where they combine to release H₂.³¹ An example of such system produced ~4.5 l H₂/day from waste water.³²

Apart from bio-electrochemical systems, hydrogen production from biomass can be light-driven. Light-dependent processes include bio-photolysis and photofermentation. In bio-photolysis, water is split to produce hydrogen by some green algae under anaerobic conditions. Photofermentation is done by using a purple non-sulfur bacteria converting organic acids into H₂ and CO₂. In light-independent processes, i.e., dark fermentation, organic substrates are converted to H₂ in anaerobic condition (Table 1).³³ With a cost of hydrogen production ranging from 1.4 to 2.8 \$/kg H₂, biological routes to process biomass are promising but are currently at a very early experimental stage.

Relative to biological routes, thermochemical methods are more flexible and provide a simpler approach as there is no need for additional chemicals but instead heat and pressure are used to generate biofuels.⁴³ This can be done by pyrolysis and/or gasification (Table 2).^{44,45} Gasification is a welldeveloped process where hydrogen-rich fuel gas (CO, H₂, and CH₄) is produced at 700-1200 °C using gasification agents (O₂, CO₂, steam, and air).^{16,20} Gasification with air produces a low-quality gas (4-7 MJ/m³ HHV), whereas higher quality gas (~10-18 MJ/m³ HHV) can be obtained under more oxidative conditions, i.e., pure O₂.⁵⁰ The gasification process using fluidized bed reactors have demonstrated high biomass conversion with H₂ content in gas ~55 vol.% and H₂ production of ~6.9 wt%.^{20,51} The cost of H₂ production by gasification from biomass is estimated to be ~1.77-2.05 \$/kg H₂,¹⁴ and the process can be generalized in the following equation:⁵²

$$Biomass \rightarrow H_2 + CO_2 + CO + N_2 \tag{2}$$

 H_2 can also be obtained via the pyrolysis of biomass at lower temperatures of 300-650 °C,^{20,52,53} but, at such temperatures, the hydrogen yield is lowered and of ~18 vol%.⁵² However, with suitable catalysts, e.g., Ni/Al₂O₃,²⁰ and elevated temperatures, the amount of produced H₂ can be increased to yields ~38 vol% at 600 °C and ~70 vol% at 900 °C. Recently, an effective twostaged pyrolysis process has been proposed,⁵⁴ where the biomass is initially heated to 950 °C to produce pyrolysis gases, and then further heated at 950 °C again. With a 10 wt % Ni-dolomite catalyst, the amount of hydrogen obtained in this two steps process was 59.14 vol%.⁵⁵ The cost of H₂ production from biomass pyrolysis has been calculated as 1.25-2.20 \$/kg H₂,¹⁴ and the process is generalized in the following equation:⁵²

Biomass
$$\rightarrow$$
 H₂ + CO₂ + CO + hydrocarbon gases (3)

Recently, other feedstocks like bioethanol, glycerol, sorbitol, and glucose have also been investigated as a potential source of hydrogen⁵⁶ through the conventional approach of steam

Process	Reactions	Organisms	Key enzymes	Substrate	H ₂ yield	\$/kg H ₂	Reactors	References
Biophotolysis	$\begin{array}{l} \textit{Direct:} \\ 2H_20 + \text{light} \rightarrow 2H_2 + 0_2 \\ \textit{Indirect:} \\ 6H_20 + 6C0_2 + \text{light} \rightarrow \\ C_6H_{12}0_6 + 6C0_2 \\ C_6H_{12}0_6 + 2H_20 \rightarrow 4H_2 \\ + 2CH_3C00H + 2C0_2 \end{array}$	Chlamydomonas reinhardtii, Chlorella fusca, Scenedesmus obliquus, Chlorococcum littorale, Nostoc, Anabaena, Calothrix, Oscillatoria	Nitrogenase or hydrogenase	Water, carbohydrate	119.8 ml/l (direct biophotolysis)	2.13 (direct) 1.42 (indirect)	Photobioreactor, flat plate photobioreactor	[14,33–36]
Photofermentation	$\begin{array}{l} C_6H_{12}O_6+6H_2O+light\\ \text{energy} \rightarrow 12H_2+6CO_2\\ \textit{Nitrogen-deficient}\\ \textit{process:}\\ CH_3COOH+2H_2O+\\ \textit{light energy} \rightarrow 2H_2+\\ 2CO_2 \end{array}$	Rhodobacter capsulatus, Rhodobium marinum, R. sphaeroides	Nitrogenase, hydrogenase	Sugar beet molasses, food waste, wastewater	1 I/I with 28 g/I sugar-containing culture, 3.65 mol/ mol mixed acids (acid and butyric acid)	2.83	Borosilicate glass bioreactors, fed batch	[14,35,37– 39]
Dark fermentation	$C_6H_{12}O_6 + 6H_2O \rightarrow 12H_2 + 6CO_2$	Bacillus, Enterobacter, Clostridium, Thermotoga, Thermoanaerobacterium	Hydrogenase	Wastewater mixed sludge, glucose, xylose	~1.7 mol/mol glucose, 0.8 mol/ mol xylose	2.57	Gass bioreactors serum bottles, fluidized bed reactors	[14,40-42]

Table 2. Hydrogen production strategies from pyrolysis and the gasification process.

Methods	Brief description	Reactor and condition	Advantage	Disadvantage	Product yield
Air gasification ^{21,24,46}	Uses air as a gasifying agent to produce CO + H ₂	Fluidized bed reactor/700– 900 °C air with steam mixture	Can achieve maximum conversion	Removal of tar from the product is difficult	High H ₂ and gas yield at high temperature
Steam gasification ^{21,24,26,47}	Uses steam along with air to produce H ₂ -rich syngas	Fluidized bed gasifier/770 °C and steam to the biomass ratio of 1	High H ₂ to CO ratio, suitable for large-scale industrial production	High tar content and CO ₂ emission	19.4-42.6% H ₂
Oxygen gasification ²⁴	Supplies pure oxygen into gasifier for gasification	Circulating fluidized bed gasifier	Low tar content in the syngas produced	Purifying oxygen is an energy-intensive process	
Supercritical water gasification ^{21,24,26,48}	Uses supercritical steam as a gasifying agent. Also, at the supercritical condition, steam works as a catalyst toward the conversion	Tubular batch reactor/650 °C with a heating range of 30 °C/ min	High conversion and H ₂ content without tar and coke formation	High energy input to pump the feed stock, strict operating condition, and difficult to recycle alkaline catalyst	30-40% H ₂
Fast pyrolysis ^{21,24,26,49}	Occurs at moderate temperature in the absence of oxygen with a high heat transfer rate to the biomass particle	Fluidized bed reactor, atmospheric pressure	Can produce high hydrogen content gas	Low hydrogen yield and high energy consumption	12% gases (2–3 wt% of H $_2$ to biomass), 72% bio-oil, 16% char

reforming¹¹:

$$C_n H_m + n H_2 O \leftrightarrow n CO + \left(\frac{m}{2} + n\right) H_2$$
 (4)

In this approach, the hydrogen content in syngas varies according to the gasification operating conditions, i.e. temperature, steam-to-biomass ratio, and catalysts. Steam gasification is prone to the formation of tar, which may affect the maintenance and operation cost due to pipeline blockage.⁵⁷ Therefore, catalysts are often used to promote tar cracking and reduce the operating temperature as well as increase the hydrogen selectivity from biomass.⁵⁸ Some of the common catalysts are alkaline earth catalysts (e.g., KOH, KHCO₃, Na₃PO₄, MgO, and NaOH),^{26,59} metal-based catalysts (e.g., Ni/Al₂O₃. Ni/Al, Ni/Zn/Al, Cu/Zn/Zr, Rh/Zr/Ce, Pt/Co/CeO₂, and Ru/SrO-Al₂O₃),⁶⁰⁻⁶⁷ and mineral catalysts (dolomite and olivine).^{68,69} The activity of the metal-based catalysts supported on Al₂O₃-MgO is in an order of Ru > Rh > Ir > Ni > Pt.⁷⁰ Although the noble metals such as Ru and Rh can effectively promote gasification, these remain expensive. Traditional alkali metal catalysts have also been used effectively; however, challenges remain due to the high loading, easy scaling, blockage, and difficult recovery. As a result, Ni-based catalysts have been widely used especially due to their synergy with other metals.

For example, 100% carbon conversion and ~70 vol% H_2 yield have been reported with a Pt-Ni/CeO₂-SiO₂ catalyst.⁷¹ With an estimated cost of H_2 production up to ~5.5 \$/kg H_2 ,⁷² more scientific advancement is needed before biomass gasification technologies can be used at an industrial scale. The future efforts are expected to be on tar treatment, cost-effective catalysts, condition optimization, and large-scale implementation.

Making hydrogen by splitting water

Even though water is an abundant hydrogen source, water electrolysis accounts for only a small fraction of the global hydrogen production.⁷³ Depending on the energy source used, water electrolysis can be a completely sustainable and a clean way to generate hydrogen since no greenhouse gas is

emitted.⁷⁴ Hydrogen production from water splitting can be done by using various methods including electrolysis and photocatalysis.⁷⁵ However, the latter is far from mature. During the photocatalysis process, a light excited semiconducting electrode with a suitable excitation bandgap, e.g., TiO₂, is used to split water into hydrogen and oxygen.⁷⁶ Unfortunately, TiO₂ strongly absorbs light in the UV spectrum ($\lambda < 350$ nm) only, and not in the visible light range (350 nm $<\lambda < 700$ nm), and this results in a poor photocatalytic activity under sunlight. The development of high-performing photocatalysts under sunlight is therefore critical for photocatalysis to become a key method to produce H_{2}^{77} To date, many semiconductor photocatalysts and co-catalysts have been studied including doped TiO₂,⁷⁸ perovskites,⁷⁹ graphitic C₃N₄,⁸⁰ BiVO₄,⁸¹ and NiS.⁸² Although this approach is reported to have less environmental impact, the poor efficiency $(10-18\%)^{83}$ and relative high cost are not attractive.⁸⁴ Early estimation would suggest a hydrogen production cost between 1.6 and 10.4 \$/kg H₂.⁸⁵

Exotic methods including sonolysis, where a sound wave between 20 and 40 kHz is used to split water through cavitation effects, have been reported.⁸⁶ Thermochemical water splitting from solar concentrators (>2000 °C) have also been proposed with relatively high efficiency (49% solar-to-fuel energy conversion efficiency).⁸⁷ Depending on the type of thermochemical cycles used (where heat sources and chemical reactions are combined to split water into hydrogen and oxygen),⁷⁵ the cost of H₂ production varies considerably from 2.8–4.1 \$/kg H₂ for the hybrid sulfur cycle,⁸⁸ to 8.0–14.7 \$/kg H₂ for the ZnO/Zn cycle,⁸⁹ and 2.2 \$/kg H₂ for the Cu-Cl cycle.⁷⁵

Electrolysis is a general term describing the process of driving a non-spontaneous electrochemical reaction by applying a voltage difference between two electrodes. In water electrolysis, gaseous hydrogen and oxygen are generated from water in the following equation:

$$2H_2O(l) \rightarrow 2H_2(g) + O_2(g) \tag{5}$$

This is an energy-demanding reaction with a change in Gibbs free energy of 237.2 kJ/mol at standard conditions.^{90,91} If this reaction is done in an electrochemical cell, a potential difference of 1.23 V is required at room temperature and standard pressure.⁹² Various electrochemical cell configurations and chemistry have been investigated to generate hydrogen through water electrolysis. These technologies are at various stages of maturity and include the proton exchange membrane (PEM),^{93,94} alkaline water (AW),^{95,96} anion exchange membrane (AEM),^{97,98} solid oxide electrolysis (SOE),⁹⁹ and microbial electrolysis cell (MEC)¹⁰⁰ technologies.

Table 3 summarizes the characteristics of these different approaches, and to date, AW electrolysis remains the most cost effective approach to generate hydrogen.¹⁰⁴⁻¹⁰⁶ PEM systems lead to the highest H₂ purity but unfortunately suffer from several limitations such as electrolyte contamination,^{107,108} and deterioration,¹⁰⁹ and slow oxygen evolution reaction (OER) kinetics.¹¹⁰ To speed up the OER kinetics,

various catalysts have been tested including Pt on carbon, ruthenium-based materials,¹¹¹ and non-noble metal catalysts¹¹²

The price and source of electricity to power the electrolysis reaction are additional factors to consider. Several projects have demonstrated the technological viability of renewable hydrogen from wind and solar. However, advancements in direct and more efficient water electrolysis processes from renewable sources are needed to reduce cost and facilitate the uptake of renewable hydrogen.¹¹³

Over the past decades, there has been a rapid increase in installed capacity of wind energy coupled with a decrease in the associated costs.¹¹⁴ It is therefore of little surprise that researchers around the planet are looking into the utilization of wind energy to produce hydrogen.¹¹⁵⁻¹¹⁸ The calculated costs involved with H₂ production from wind energy vary widely based on several factors including if the wind-mills are gridconnected or isolated systems, the type of electrolysers used, and wind penetration scenarios.¹¹⁹ For example, a Norwegian study calculated prices between 2.0 and 4.5 \$/kg H₂,¹¹⁵ a Danish study predicted a price of around 3.5 \$/kg H₂,¹¹⁹ whereas a South African study listed values between 1.4 and 39.5 \$/kg H₂.¹¹⁶ The annual hydrogen production volume also varies considerably based on the country's available wind energy capacity and the mean wind speed. In Fayzabad, Afghanistan, a 100 kW wind turbine system could produce up to 8.7×10^6 kg H₂/year,¹¹⁷ in South Africa, between 6.5×10^3 and 2.3×10^5 kg H₂/year could be generated, ¹¹⁶ while in Brazil the projected hydrogen production from the surplus wind electricity was predicted to be of 2.2×10^{11} kg H₂/year.¹¹⁸

Producing hydrogen from photovoltaics (PV) was once the most expensive method (up to $78.6 \text{ }/\text{kg H}_2$) due to the high cost of the PV system.¹²⁰ However, installed solar capacity has increased drastically due to the recent sharp drop in price of solar PV systems.¹²¹ To date, solar is the most cost-competitive way to produce clean renewable hydrogen.¹²² In 2007, a study calculated that a PV electrolysis plant of 260 km² would be enough to provide an annual H₂ production of 2.2×10^8 kg at a cost of 6.5 \$/kg H₂,¹²³ and since then, the cost of solar hydrogen has fallen to less than 3 \$/kg H₂.¹²⁴ Solar hydrogen production capacity and the cost of course depend on multiple factors including the country and location (solar irradiation level), the type of electrolysers, and the nature of the PV systems, i.e., gridconnected or autonomous.¹²² For example, it has been predicted that a 20 kW PV system receiving 299 MW/h of solar radiation would produce 3.73×10^5 kg H₂/year,¹²⁵ while a Japanese study projected a low production cost of 1.7-2.8 \$/ kg using a PV and battery-assisted electrolysers.¹²⁴ As compared with solar, wind energy has the advantage of being a "dual-use" technology where the land can still be used for other important activities such as farming and agriculture, or even solar farms. Hybrid wind-solar systems could be one solution in order to maximize the use of land and minimize the problem of intermittent solar irradiation.¹²⁶⁻¹²⁸ Floating systems could also provide alternatives to produce hydrogen while minimizing land impact.129

Table 3. Materials, components, and characteristics of different electrolysis systems.

	Alkaline ^{101,102}	PEM ^{101,102}	AEM ^{101,103}
Electrolyte	20—30% KOH	PFSA	QAPS
Charge carrier	OH-	H+	OH-
Temperature range (°C)	65–100	70–100	50–70
Typical discharge H ₂ pressure (bar)	25–30	30–80	30
Separator	Asbestos, PAMa, ZrO ₂ –PPS, NiO, Sb ₂ O ₅ –PS	PFSA (e.g., Nafion)	QAPS (e.g., A—201)
OER catalyst	Ni ₂ CoO ₄ , La–Sr–CoO ₃ , Co ₃ O ₄	Ir/Ru oxide	C0 ₃ 0 ₄
HER catalyst	Ni	Pt	CeO ₂ -La ₂ O ₃
Typical current collector	Ni	Titanium	Ni
Cell sealant	Metallic	Synthetic rubber or fluoroelastomer	Synthetic rubber or fluoroelastomer
Anodic reaction	$20H^- \rightarrow H_20 + 1/20_2 + e^-$	$2\mathrm{H}_{2}\mathrm{O}\rightarrow\mathrm{O}_{2}+4\mathrm{H}^{+}+4\mathrm{e}^{-}$	$20H^- \rightarrow H_20 + 1/20_2 + e^-$
Cathodic reaction	$2\mathrm{H}_{2}\mathrm{O}+2\mathrm{e}^{-}\rightarrow2\mathrm{H}_{2}+2\mathrm{OH}^{-}$	$4\mathrm{H^{+}} + 4\mathrm{e^{-}} \rightarrow 4\mathrm{H_{2}}$	$2\mathrm{H}_{2}\mathrm{O}+2\mathrm{e}^{-}\rightarrow2\mathrm{H}_{2}+2\mathrm{OH}^{-}$
Conventional current density (mA/ cm ²)	200–500	800–2500	200–500
Demonstrated durability (h)	100,000	100,000–50,000	NA
Hydrogen purity (%)	99.3–99.9	99.9999	99.99
Typical current efficiency	50–70.8	48.5–65.5	39.7
Demonstrated rated production (N m ³ /h)	1–760	0.265–30	0.25–1
Specific energy consumption (kWh N/m ³)	4.5–7.5	5.8–7.3	5.2-4.8
Demonstrated rated power (kW)	2.8–3534	1.8–174	1.3–4.8
System cost (\$/kg)	1400–900	2200–1300	NA
Technology status	Mature for large scale	Mature for small scale	R&D

PAMa: polysulphone-bonded polyantimonic acid; PPS: ZrO_2 on polyphenylsulphone; Sb_2O_5 -PS: polysulphone impregnated with Sb_2O_5 polyoxide; PFSA: perflurosulfonated acid; QAPS: quaternary ammonia polysulfone; OER: oxygen evolution reaction; HER: hydrogen evolution reaction; NA: not available.

Alternatives including hydropower and geothermal may also have the potential to be used to produce hydrogen. Hydropower is often considered expensive due to the upfront capital cost of building huge dams. However, a Canadian study found that despite the initial capital costs, hydropower H_2 production is cost competitive as compared with steam methane reforming

at 2.4 $k/kg H_2$, and if the upfront investments are excluded (by using existing hydropower plants), the hydrogen cost goes down to 1.2 $k/kg H_2$.¹³⁰ Geothermal energy is another source of sustainable energy, and a recent study demonstrated that geothermal powered electrolysis is a viable method for hydrogen production (1.1 $k/kg H_2$) with a payback period of only 4-5 years.¹³¹

Storage and distribution of hydrogen

Effective methods to store hydrogen are essential to enable its widespread utilization in particular for industrial use where plants require a constant feedstock input. The main problem with storing hydrogen is its low volumetric density. Hydrogen is the lightest element, and at ambient condition, it is a gas with a low density of 0.0899 kg/m³.¹³² Even when liquefied at -253 °C, the density of H₂ is only 70.8 kg/m³, which is onefifteenth of water's density. Hydrogen is also a very small highly diffusive molecule and thus hydrogen leaks can easily occur.¹³³ Besides, the use of hydrogen is associated with difficulties in terms of materials' compatibility. In particular, the dissociation of hydrogen molecules at the surface of metals and further hydrogen diffusion at metallic interstitial sites can lead to piping embrittlement and accidental fracture as a result of the reduced ductility and weakening of metals subjected to high purity/pressure hydrogen.¹³⁴⁻¹³⁶ The storage of hydrogen is also more delicate than other fuels, because hydrogen has higher laminar burning, buoyant, and propagation velocities that results in higher flammability than other fuels. In addition, hydrogen is also very sensitive to detonation due to its wide volume fraction range of ignition (4-74%) and detonation (18-59%).¹³⁷⁻¹⁴⁰

Existing methods to store hydrogen are summarized in Fig. 5. Storing hydrogen in high pressure vessels (up to 700 bar in lightweight composite cylinder) is the most common method so far, but the resulting low volumetric storage density, high cost of the composite vessels (~\$13/KWh for 100,000 vessels per year),¹⁴¹ and their maintenance/safety are still a concern.¹⁴⁰ Cryogenic tanks are designed to store liquid hydrogen at -253 °C under ambient pressure (the pressure can increase to 10^4 bar in a closed storage system due to the low critical temperature (-239.95 °C) of hydrogen).¹⁴² As a general observation and depending on the vessel design, conventional cryogenic tanks can store twice more hydrogen per volume as compared to 700 bar hydrogen gas tanks.¹⁴² However, with such a storage technology, it is inevitable to avoid the loss of hydrogen even with a perfect insulation because of heat leakage.^{143,144} The boiling losses of 0.4% per day for a 50 m³ double-walled vacuum-insulated spherical Dewar vessel have been reported.¹⁴⁵ In addition, hydrogen liquefaction is a very energy intensive process with at least 30% of the energy stored lost through the liquefaction of hydrogen.¹⁴⁶

Hydrogen can also be stored by materials physically or chemically. This includes microporous materials, interstitial metal hydrides, and complex hydrides. Microporous materials, including carbon materials, ¹⁴⁷⁻¹⁵² zeolites, ¹⁵³⁻¹⁵⁸ and metal organic frameworks (MOFs), ¹⁵⁹⁻¹⁶³ can absorb molecular hydrogen in their porous structures at low temperature. ^{152,164,165} The hydrogen storage capacity then depends upon the specific surface areas and the applied pressure. ^{142,152} Typically, the adsorption capacity of MOFs is <2 wt% at room temperature. ¹⁶⁶ The advantage of porous materials is that they allow for hydrogen storage at higher temperatures, e.g., -150 °C, than feasible with cryogenic tanks for the similar volumetric hydrogen densities. ¹⁴³



Electricity steel mill chemical processes



An alternative method to store hydrogen is in the use of materials storing hydrogen within their structure to form a hydride. Metal hydrides are usually formed by the reaction between metals or intermetallic compounds with hydrogen by the reversible reaction below¹⁶⁷:

$$M_{(s)} + x/2H_{2(g)} \leftrightarrow MH_{(S)} + Q$$
 (6)

where M is either a metal, an alloy, or an intermetallic compound, MH is the metal hydride formed, and Q is the heat generated during the reaction.¹⁶⁷

Interstitial metal hydrides are capable of absorbing large amounts of hydrogen (i.e., the volumetric density of LaNi₅ is 123 kg H₂/m³ of material; that is 1.74 times more than that of liquid hydrogen). In this process, hydrogen is stored in an atomic form after dissociation of molecular hydrogen at the surface of the interstitial metal.¹⁴⁷

Generally, existing binary hydrides along the periodic table of elements are too unstable or too stable to be relevant for practical application. However, it has been found that intermetallic compounds, e.g., TiFe, ZrV₂, and LaNi₅,^{166,168,169} formed by alloying at least two elements (one unstable with one stable hydride) can facilitate the hydrogen storage properties. Generally, the element forming a stable hydride are transition metals or rare earths like Ti, Zr, Y, and La. The unstable hydride elements (often absorbing hydrogen at high hydrogen pressure only) are transition metals including Cr, Mn, Fe, Co, and Ni. The formation of intermetallic alloyed by these two elements can lead to intermediate hydrogen sorption properties with reversibility. Interstitial metal hydrides show excellent and practical hydrogen storage properties since they can uptake and release a large amount of hydrogen safely at ambient temperature and moderate hydrogen pressures.¹⁷⁰ However, one of the major limitations of these interstitial hydrides is their weight, because their composition involves heavy elements, and this results in low gravimetric hydrogen storage capacities.

Better hydrogen storage materials, i.e., of higher gravimetric storage capacities, may exist in the form of complex hydrides. Complex hydrides are ionic compounds that release hydrogen when they decompose.¹⁷⁰ Complex hydrides are usually formed through the combination of alkali or alkaline earth metals, e.g., Li, Na and Mg, and $[AlH_4]^-$, $[NH_2]^-$ and $[BH_4]^-$ groups. The theoretical gravimetric and volumetric densities of some of the complex hydrides are high, for example, the theoretical gravimetric capacity of LiBH4 is 18.5% and the volumetric capacity is $121 \text{ kg H}_2/\text{m}^3$ (70% more than the volumetric capacity of liquid hydrogen).¹⁷¹⁻¹⁷³ However, the multiple steps of hydrogen desorption, the release of impurities in the form of B₂H₆ from borohydrides or NH₃ from amides, and the poor hydrogen reversibility of these materials remain the main barrier for their practical applications. The poor reversibility is generally due to the formation of stable intermediate decomposition products during decomposition and extensive elemental disproportion.¹⁶⁶ Different strategies including those based on the potential to alter the properties of hydrogen in nanohydride materials are under current investigations to tackle these challenges.¹⁶⁶

Currently, hydrogen is delivered from production sites to the end-users including refueling stations by road or pipeline depending on the application, volume, and distance.¹⁷⁴ For small volumes, transport by road remains the most favorable option. In this case, hydrogen is compressed to 180–200 bar and delivered by tube trailers. Delivering liquid hydrogen is more economical over long distances due to the higher volumetric density. A 40 ton truck can carry 350 kg of gaseous hydrogen or 3500 kg liquid hydrogen,¹⁴³ and the delivery cost of compressed hydrogen gas is \$1/kg/100 km by tube trailers and \$0.1/kg/100 km for liquid hydrogen by trucks in the USA.¹⁷⁵ Hydrogen is also noncorrosive; therefore, this facilitates the design and construction of tank trailers. However, because of the extreme low temperature, additional space for safety and suitable thermal insulation must be considered.^{138,143}

Gaseous hydrogen can also be transported in pipelines like natural gas, especially when large volumes are to be transported over long distances. In this case, the cost of hydrogen transport is estimated to be of $0.1/\text{kg H}_2$ over 100 km.¹³⁸ However, this does not take into account the need to retrofit exiting gas network. Conventional pipelines for natural gas are made of steel with a typical diameter of 25-30 cm and the operation pressure is 10-20 bar.¹⁴² Using such an infrastructure to transport hydrogen is not feasible in many cases without substantial modifications to reduce diffusion losses in sealing areas as well as materials and seals embrittlement.¹⁴³ In addition, the minimum power required to pump a gas through the pipe follows the equation below:

$$P = 8\pi l v^2 \eta \tag{7}$$

where *l* is the length of the pipe, and *v* and η are the velocity and dynamic viscosity of the gas. The volumetric density of hydrogen is 36% of the density of natural gas at the same pressure, and the viscosity of hydrogen is 80% of that of natural gas. Therefore, to pump the same amount of hydrogen, the power needed is 2.2 times that for natural gas.¹⁴²

The role of enabling policies

Today, hydrogen is mainly used for the production of ammonia and hydrocracking processes, with only a small portion used in the transport sector including in the nascent fleet of fuel cell vehicles. Uncertainties in technological development and price advantage of fossil fuel present a major challenge for the growth of renewable hydrogen at the industrial scale. Industry faces national and international competitive pressures, and existing economic models are highly sensitive to feedstock prices. Projections from the International Partnership for the Hydrogen Economy (IPHE) assume that hydrogen will continue to be produced from cheaper fossil fuels before renewable hydrogen can play a significant role. However, continuing declining prices of wind turbines,¹⁷⁶ solar PV,¹⁷⁷ and electrolysers¹⁷⁸ suggests that the production of hydrogen via power-to-gas (PtG) may become economically favorable in the next decade.¹⁷⁹ For example, case studies have found that renewable hydrogen is already cost competitive in small- and mediumscaled applications combining renewable wind energy with a PtG facility.¹⁷⁹ In this transition, it is often envisaged that carbon capture and storage may assist the production of low-carbon emission hydrogen from natural gas and coal, although currently not competitive.¹⁸⁰ Solutions still remain to be found to effectively capture and store carbon dioxide, without mentioning the social licence aspects of such a solution.¹⁸⁰

Additionally, non-economic barriers hindering the deployment of hydrogen technologies and infrastructures have also been identified.¹⁸¹ This includes (i) complex procedures and lack of information and assistance to enable projects, (ii) lack of public knowledge and awareness of the renewable hydrogen, (iii) social acceptance of the safety of hydrogen-related technologies and infrastructures, and (iv) lack of government initiatives to facilitate the use of hydrogen technologies and infrastructure construction. Existing safety regulations along hydrogen production, distribution, and storage are also limiting factors.¹⁸²

In recent years, many countries have announced ambitious initiatives and visions to utilize renewable hydrogen as an energy carrier and achieve the greenhouse gas emission targets following the Paris Agreement in November 2016.¹⁸³ However, implementation toward an hydrogen economy is still distant and in the light of the COVID-19 pandemic lobbying toward business as usual is more than ever prevalent. Currently, there are more than 19 hydrogen strategies and roadmaps around the world.¹⁸⁴ However, many countries aim to focus on hydrogen use across the transport sector and existing gas distribution and transmission networks, with little understanding of the potential of hydrogen in the industrial sector. The EU, France, and Norway in contrast have identified hydrogen as an industrial feedstock, and aims to focus their strategy in this area, ¹⁸⁴ while the transport sector is to remain mainly battery-driven.

Policy and pilot projects that could enable the use of renewable hydrogen in industry are still lacking because of the relativity high cost of renewable hydrogen (approximately 5.30 /kg H₂).¹⁸⁵ Only a few countries offer subsidies, tax incentives, and rebates for investments in renewable hydrogen production. For example, in Norway, electricity used to electrolyse water for hydrogen production is tax exempt, and in the Netherlands, a subsidy of up to ϵ 750,000 supports hydrogen-related projects.¹⁸²

Many of the current demonstration and commercialization projects along renewable hydrogen plants are initiated by industry only, with the private sector expected to invest more than \$50 billion in hydrogen projects by 2030. For example, Shell and ITM Power planned to install a 10 MW electrolyser in its refining industry site in Germany in 2017. In many countries like the USA, Japan, and China, primary hydrogen investments remain toward the deployment of fuel cell vehicles and hydrogen refuelling stations. While the heavy industry sector is the largest consumer of hydrogen, this sector is more closely bound to emission reduction regulations, renewable energy mandates, and carbon markets, compared with other light industries.¹⁸⁶

Currently, there is no standard for low-carbon hydrogen, and green hydrogen is not recognized as a renewable fuel in many countries and thus not accountable toward the renewable target set in the mobility sector. It is therefore essential for organizations and policymakers to develop appropriate national and international standards, regulations, and relevant hydrogen certifications. This will allow renewable hydrogen to be supported by climate policies, in the same way as renewable technologies. The system "CertifHy" proposed in Europe to evaluate the environmental value of hydrogen could be a starting model to trade certified hydrogen. In this system, CO₂ emission levels (91 g CO₂/MJ H₂) of hydrogen produced from reforming natural gas are used as a reference point. Hydrogen produced with a 60% reduction from this level (i.e., 36.4 g CO₂/MJ H₂) is defined as "Premium Hydrogen," while Premium hydrogen produced from renewable energy is defined as "Green Hydrogen."187

Government policies need to be designed as a long-term and fair competition platform for the hydrogen sector, introducing both incentives and regulations. When designing regulations relating to greenhouse gases reduction for industry, it is essential to acknowledge the significance and feasibility of clean hydrogen. It is conceivable to make use of a certain percentage of clean hydrogen in industrial processes mandatory with targeted reductions in use of steam methane-reforming hydrogen. Meanwhile, long-term high-risk mitigation implementations and incentives, such as the subsidy of a percentage of the high capital expenditure or compensation via products, could be effective in stimulating the large-scale production and supply of clean hydrogen. This can possibly reduce the cost of clean hydrogen for consumers, accelerating its mass deployment across industry.

Finally, public awareness and acceptance toward hydrogen are also important factors. It is apparent that many citizens are not educated on the potential of renewable hydrogen and its benefits for the environment.¹⁸¹ Even though the social acceptance of new technologies is considerably high in many European countries, hydrogen is still considered dangerous due to its high flammability. It is therefore important to demonstrate and implement a production of hydrogen that is safe to gain an increase in public support.

Summary and perspectives

As a crucial reactant for the chemical industry, the demand for hydrogen has grown considerably and will continue to rise in the foreseeable future. However, with most of the industrial hydrogen being sourced from fossil fuels, it is imperative that we start looking into sustainable production methods for hydrogen to succeed as a clean chemical feedstock and an energy carrier. Currently, only a small fraction of hydrogen is produced from renewable sources due to slow technological advances, lack of mass scale manufacturing of hydrogen technologies, and thus a high cost of green hydrogen relative to fossil fuels, and the lack of environmental government policies promoting

the use of clean hydrogen. A few emerging technologies look promising based on the 2020 DOE target and even appear cost competitive to steam methane reforming for hydrogen production. However, the calculated production costs often do not tell the whole story; for example, electrolysis via geothermal and hydropower has a low cost of 1.1-2.4 \$/kg H₂ but unfortunately their use is restricted by the geographic location of the energy source. Biochemically processed biomass also appears cost competitive at 1.4-2.8 \$/kg H2, but as an emerging technology, its reliability and actual cost at an industrial scale still remains to be determined. So far, wind-powered water electrolysis appears to have the best chance to play a major role in renewable hydrogen production due to the maturity and decreasing cost of wind technology. Once produced, the last hurdle for hydrogen is its storage and transport due to the low density of the gas. Until new methods like solid-state storage become more established, conventional methods (compressed gas cylinders and liquefied hydrogen) will remain the norm to get hydrogen to its end applications. Advancements in technological processes, cost, and policies still need to be conjointly progressed before renewable hydrogen can become the mainstream.

REFERENCES:

- 1. IEA: The Future of Hydrogen (International Energy Agency, 2019), Paris.
- Klerke A., Christensen C.H., Nørskov J.K., and Vegge T.: Ammonia for hydrogen storage: Challenges and opportunities. *J. Mater. Chem.* 18, 2304 (2008).
- Navarro R.M., Peña M.A., and Fierro J.L.G.: Hydrogen production reactions from carbon feedstocks: Fossil fuels and biomass. *Chem. Rev* 107, 3952 (2007).
- International Council of Chemical Associations DECHEMA: Technology Roadmap: Energy and GHG Reductions in the Chemical Industry Via Catalytic Processes (International Energy Agency (IEA), 2013), Paris, France.
- Veldsink J.W., Bouma M.J., Schöön N.H., and Beenackers A.A.C.M.: Heterogeneous hydrogenation of vegetable oils: A literature review. *Catal. Rev.* 39, 253 (1997).
- 6. Allen R.R.: Hydrogenation. J. Am. Oil Chem. Soc. 58, 166 (1981).
- 7. Wurster O.H.: Hydrogenation of fats. Ind. Eng. Chem. 32, 1193 (1940).
- Dhaka V., Gulia N., Ahlawat K.S., and Khatkar B.S.: Trans fats sources, health risks and alternative approach – A review. *J. Food Sci. Technol.* 48, 534 (2011).
- Lee I., Delbecq F., Morales R., Albiter M.A., and Zaera F.: Tuning selectivity in catalysis by controlling particle shape. *Nat. Mater.* 8, 132 (2009).
- Philippaerts A., Jacobs P.A., and Sels B.F.: Is there still a future for hydrogenated vegetable oils? *Angew. Chem. Int. Ed.* 52, 5220 (2013).
- Demirbas A.: Hydrogen production from carbonaceous solid wastes by steam reforming. *Energy Sources A* 30, 924 (2008).
- Hosseini S.E. and Wahid M.A.: Hydrogen production from renewable and sustainable energy resources: Promising green energy carrier for clean development. *Renew. Sustain. Energy Rev.* 57, 850 (2016).
- Lemus R.G. and Martínez Duart J.M.: Updated hydrogen production costs and parities for conventional and renewable technologies. *Int. J. Hydrogen Energy* 35, 3929 (2010).
- M. Kayfeci, A. Keçebaş and M. Bayat: Chapter 3 Hydrogen production. In Solar Hydrogen Production, Calise F., D'Accadia M.D., Santarelli M., Lanzini A. and Ferrero D., eds. (Academic Press, Cambridge, Massachusetts, US, 2019), p. 45.
- El-Emam R.S. and Özcan H.: Comprehensive review on the techno-economics of sustainable large-scale clean hydrogen production. *J. Clean. Prod.* 220, 593 (2019).

- Granados-Fernández R., Cortés-Reyes M., Poggio-Fraccari E., Herrera C., Larrubia MÁ, and Alemany L.J.: Biomass catalytic gasification performance over unsupported Ni-Ce catalyst for high-yield hydrogen production. *Biofuel. Bioprod. Bioresour.* 14, 20 (2019).
- Resasco D.E., Wang B., and Sabatini D.: Distributed processes for biomass conversion could aid UN Sustainable Development Goals. *Nat. Catal.* 1, 731 (2018).
- Navarro R.M., Sanchez-Sanchez M.C., Alvarez-Galvan M.C., del Valle F., and Fierro J.L.G.: Hydrogen production from renewable sources: Biomass and photocatalytic opportunities. *Energy Environ. Sci.* 2, 35 (2009).
- Kalinci Y., Hepbasli A., and Dincer I.: Life cycle assessment of hydrogen production from biomass gasification systems. *Int. J. Hydrogen Energy* 37, 14026 (2012).
- Arregi A., Amutio M., Lopez G., Bilbao J., and Olazar M.: Evaluation of thermochemical routes for hydrogen production from biomass: A review. *Energy Convers. Manage.* 165, 696 (2018).
- Dou B.L., Zhang H., Song Y.C., Zhao L.F., Jiang B., He M.X., Ruan C.J., Chen H.S., and Xu Y.J.: Hydrogen production from the thermochemical conversion of biomass: Issues and challenges. *Sust. Energy Fuels* 3, 314 (2019).
- Demirbas A.: Biorefineries: Current activities and future developments. *Energy Convers. Manage.* 50, 2782 (2009).
- Zheng X., Ying Z., Wang B., and Chen C.: Hydrogen and syngas production from municipal solid waste (MSW) gasification via reusing CO₂. *Appl. Therm. Eng.* 144, 242 (2018).
- Pandey B., Prajapati Y.K., and Sheth P.N.: Recent progress in thermochemical techniques to produce hydrogen gas from biomass: A state of the art review. *Int. J. Hydrogen Energy* 44, 25384 (2019).
- Formica M., Frigo S., and Gabbrielli R.: Development of a new steady state zero-dimensional simulation model for woody biomass gasification in a full scale plant. *Energy Convers. Manage.* 120, 358 (2016).
- Cao L., Yu I.K.M., Xiong X., Tsang D.C.W., Zhang S., Clark J.H., Hu C., Ng Y.H., Shang J., and Ok Y.S.: Biorenewable hydrogen production through biomass gasification: A review and future prospects. *Environ. Res.* 186, 109547 (2020).
- Mahidhara G., Burrow H., Sasikala C., and Ramana C.V.: Biological hydrogen production: Molecular and electrolytic perspectives. *World J. Microbiol. Biotechnol.* 35, 116 (2019).
- Hallenbeck P.C. and Benemann J.R.: Biological hydrogen production: Fundamentals and limiting processes. *Int. J. Hydrogen Energy* 27, 1185 (2002).
- Hirose A., Kasai T., Aoki M., Umemura T., Watanabe K., and Kouzuma A.: Electrochemically active bacteria sense electrode potentials for regulating catabolic pathways. *Nat. Commun.* 9, 1083 (2018).
- Hirose A., Kasai T., Koga R., Suzuki Y., Kouzuma A., and Watanabe K.: Understanding and engineering electrochemically active bacteria for sustainable biotechnology. *Bioresour. Bioprocess.* 6 (2019).
- Kadier A., Simayi Y., Abdeshahian P., Azman N.F., Chandrasekhar K., and Kalil M.S.: A comprehensive review of microbial electrolysis cells (MEC) reactor designs and configurations for sustainable hydrogen gas production. *Alex. Eng. J.* 55, 427 (2016).
- Baeza J.A., Martínez-Miró À, Guerrero J., Ruiz Y., and Guisasola A.: Bioelectrochemical hydrogen production from urban wastewater on a pilot scale. J. Power Sources 356, 500 (2017).
- Sun Y., He J., Yang G., Sun G., and Sage V.: A review of the enhancement of bio-hydrogen generation by chemicals addition. *Catalysts* 9, 353 (2019).
- Tamburic B., Dechatiwongse P., Zemichael F.W., Maitland G.C., and Hellgardt K.: Process and reactor design for biophotolytic hydrogen production. *Phys. Chem. Chem. Phys.* 15, 10783 (2013).
- Jabbari B., Jalilnejad E., Ghasemzadeh K., and Iulianelli A.: Recent progresses in application of membrane bioreactors in production of biohydrogen. *Membranes* 9, 100 (2019).
- Fakhimi N. and Tavakoli O.: Improving hydrogen production using co-cultivation of bacteria with *Chlamydomonas reinhardtii* microalga. *Mater. Sci. Energy Technol.* 2, 1 (2019).
- Kars G. and Alparslan Ü: Valorization of sugar beet molasses for the production of biohydrogen and 5-aminolevulinic acid by *Rhodobacter*

sphaeroides O.U.001 in a biorefinery concept. Int. J. Hydrogen Energy 38, 14488 (2013).

- Ghosh S., Dairkee U.K., Chowdhury R., and Bhattacharya P.: Hydrogen from food processing wastes via photofermentation using purple non-sulfur bacteria (PNSB) - A review. *Energy Convers. Manage.* 141, 299 (2017).
- Zagrodnik R. and Laniecki M.: Hydrogen production from starch by co-culture of *Clostridium acetobutylicum* and *Rhodobacter sphaeroides* in one step hybrid dark- and photofermentation in repeated fed-batch reactor. *Bioresour. Technol.* 224, 298 (2017).
- Słupek E., Kucharska K., and Gębicki J.: Alternative methods for dark fermentation course analysis. SN Appl. Sci. 1, 469 (2019).
- Pendyala B., Chaganti S.R., Lalman J.A., Shanmugam S.R., Heath D.D., and Lau P.C.K.: Pretreating mixed anaerobic communities from different sources: Correlating the hydrogen yield with hydrogenase activity and microbial diversity. *Int. J. Hydrogen Energy* 37, 12175 (2012).
- Dessi P., Porca E., Waters N.R., Lakaniemi A.-M., Collins G., and Lens P.N.L.: Thermophilic versus mesophilic dark fermentation in xylose-fed fluidised bed reactors: Biohydrogen production and active microbial community. *Int. J. Hydrogen Energy* 43, 5473 (2018).
- Saghir M., Rehan M., and Nizami A.-S.: Recent Trends in Gasification Based Waste-to-Energy, Yongseung Yun, ed. (IntechOpen, London, UK, 2018).
- Gai C., Guo Y., Liu T., Peng N., and Liu Z.: Hydrogen-rich gas production by steam gasification of hydrochar derived from sewage sludge. *Int. J. Hydrogen Energy* 41, 3363 (2016).
- Shahbaz M., Yusup S., Inayat A., Patrick D.O., and Ammar M.: The influence of catalysts in biomass steam gasification and catalytic potential of coal bottom ash in biomass steam gasification: A review. *Renew. Sustain. Energy Rev.* 73, 468 (2017).
- Lv P.M., Xiong Z.H., Chang J., Wu C.Z., Chen Y., and Zhu J.X.: An experimental study on biomass air-steam gasification in a fluidized bed. *Bioresour. Technol.* 95, 95 (2004).
- Rapagnà S., Jand N., Kiennemann A., and Foscolo P.U.: Steam-gasification of biomass in a fluidised-bed of olivine particles. *Biomass Bioenergy* 19, 187 (2000).
- Kang K., Azargohar R., Dalai A.K., and Wang H.: Hydrogen production from lignin, cellulose and waste biomass via supercritical water gasification: Catalyst activity and process optimization study. *Energy Convers. Manage*. 117, 528 (2016).
- Iribarren D., Peters J.F., and Dufour J.: Life cycle assessment of transportation fuels from biomass pyrolysis. *Fuel* 97, 812 (2012).
- Schuster G., Löffler G., Weigl K., and Hofbauer H.: Biomass steam gasification - An extensive parametric modeling study. *Bioresour. Technol.* 77, 71 (2001).
- Gil J., Corella J., Aznar M.P., and Caballero M.A.: Biomass gasification in atmospheric and bubbling fluidized bed: Effect of the type of gasifying agent on the product distribution. *Biomass Bioenergy* 17, 389 (1999).
- Balat M.: Hydrogen-rich gas production from biomass via pyrolysis and gasification processes and effects of catalyst on hydrogen yield. *Energy Sources A* 30, 552 (2008).
- Anca-Couce A.: Reaction mechanisms and multi-scale modelling of lignocellulosic biomass pyrolysis. *Prog. Energy Combust. Sci.* 53, 41 (2016).
- Duman G. and Yanik J.: Two-step steam pyrolysis of biomass for hydrogen production. *Int. J. Hydrogen Energy* 42, 17000 (2017).
- Waheed Q.M.K. and Williams P.T.: Hydrogen production from high temperature pyrolysis/steam reforming of waste biomass: Rice husk, sugar cane bagasse, and wheat straw. *Energy Fuels* 27, 6695 (2013).
- L. He, J. Yang and D. Chen: Hydrogen from biomass: advances in thermochemical processes. In *Renewable Hydrogen Technologies Production, Purification, Storage, Applications and Safety*, Luis Gandia, ed. (Elsevier, Amsterdam, Netherlands, 2013), pp. 111.
- 57. Qiu P., Du C., Liu L., and Chen L.: Hydrogen and syngas production from catalytic steam gasification of char derived from ion-exchangeable Na- and Ca-loaded coal. *Int. J. Hydrogen Energy* 43, 12034 (2018).
- Cao L., Chen H., Tsang D.C.W., Luo G., Hao S., Zhang S., and Chen J.: Optimizing xylose production from pinewood sawdust through dilute-phosphoric-acid hydrolysis by response surface methodology. *J. Clean. Prod.* 178, 572 (2018).

- Ebadi A.G., Hisoriev H., Zarnegar M., and Ahmadi H.: Hydrogen and syngas production by catalytic gasification of algal biomass (*Cladophora glomerata* L.) using alkali and alkaline-earth metals compounds. *Environ. Technol.* 40, 1178 (2019).
- Bobadilla L.F., Álvarez A., Domínguez M.I., Romero-Sarria F., Centeno M.A., Montes M., and Odriozola J.A.: Influence of the shape of Ni catalysts in the glycerol steam reforming. *Appl. Catal. B* 123–124, 379 (2012).
- Sun J., Mei D., Karim A.M., Datye A.K., and Wang Y.: Minimizing the formation of coke and methane on Co nanoparticles in steam reforming of biomass-derived oxygenates. *ChemCatChem* 5, 1299 (2013).
- Nieva M.A., Villaverde M.M., Monzón A., Garetto T.F., and Marchi A.J.: Steam-methane reforming at low temperature on nickel-based catalysts. *Chem. Eng. J.* 235, 158 (2014).
- Men Y. and Yang M.: SMSI-like behavior and Ni promotion effect on NiZnAl catalysts in steam reforming of methanol. *Catal. Commun.* 22, 68 (2012).
- Zhang L., Pan L., Ni C., Sun T., Zhao S., Wang S., Wang A., and Hu Y.: CeO₂-ZrO₂-promoted CuO/ZnO catalyst for methanol steam reforming. *Int. J. Hydrogen Energy* 38, 4397 (2013).
- Li D., Tamura M., Nakagawa Y., and Tomishige K.: Metal catalysts for steam reforming of tar derived from the gasification of lignocellulosic biomass. *Bioresour. Technol.* 178, 53 (2015).
- 66. Iulianelli A., Palma V., Bagnato G., Ruocco C., Huang Y., Veziroğlu N.T., and Basile A.: From bioethanol exploitation to high grade hydrogen generation: Steam reforming promoted by a Co-Pt catalyst in a Pd-based membrane reactor. *Renew. Energy* 119, 834 (2018).
- Iida H., Noguchi K., Numa T., Igarashi A., and Okumura K.: Ru/12SrO-7Al₂O₃ (S12A7) catalyst prepared by physical mixing with Ru (PPh₃)₃Cl₂ for steam reforming of toluene. *Catal. Commun.* 72, 101 (2015).
- Basu S. and Pradhan N.C.: Selective production of hydrogen by acetone steam reforming over Ni-Co/olivine catalysts. *React. Kinet. Mech. Catal.* 127, 357 (2019).
- Ma X., Zhao X., Gu J., and Shi J.: Co-gasification of coal and biomass blends using dolomite and olivine as catalysts. *Renew. Energy* 132, 509 (2019).
- Wu H., La Parola V., Pantaleo G., Puleo F., Venezia A., and Liotta L.: Ni-based catalysts for low temperature methane steam reforming: Recent results on Ni-Au and comparison with other Bi-metallic systems. *Catalysts* 3, 563 (2013).
- Palma V., Ruocco C., Meloni E., and Ricca A.: Renewable hydrogen from ethanol reforming over CeO₂-SiO₂ based catalysts. *Catalysts* 7, 226 (2017).
- Marcoberardino G.D., Vitali D., Spinelli F., Binotti M., and Manzolini G.: Green hydrogen production from raw biogas: A techno-economic investigation of conventional processes using pressure swing adsorption unit. *Processes* 6, 19 (2018).
- Ewan B.C.R. and Allen R.W.K.: A figure of merit assessment of the routes to hydrogen. Int. J. Hydrogen Energy 30, 809 (2005).
- 74. Chi J. and Yu H.: Water electrolysis based on renewable energy for hydrogen production. *Chinese J. Catal.* 39, 390 (2018).
- Safari F. and Dincer I.: A review and comparative evaluation of thermochemical water splitting cycles for hydrogen production. *Energy Convers. Manage.* 205, 112182 (2020).
- Colón G.: Towards the hydrogen production by photocatalysis. *Appl. Catal.* 518, 48 (2016).
- Ismail A.A. and Bahnemann D.W.: Photochemical splitting of water for hydrogen production by photocatalysis: A review. *Sol. Energy Mater. Sol. Cells* 128, 85 (2014).
- Samokhvalov A.: Hydrogen by photocatalysis with nitrogen codoped titanium dioxide. *Renew. Sustain. Energ. Rev.* 72, 981 (2017).
- Castelli I.E., Landis D.D., Thygesen K.S., Dahl S., Chorkendorff I., Jaramillo T.F., and Jacobsen K.W.: New cubic perovskites for one- and two-photon water splitting using the computational materials repository. *Energy Environ. Sci.* 5, 9034 (2012).
- Cao S. and Yu J.: g-C₃N₄-based photocatalysts for hydrogen generation. J. Phys. Chem. Lett. 5, 2101 (2014).
- Li R., Han H., Zhang F., Wang D., and Li C.: Highly efficient photocatalysts constructed by rational assembly of dual-cocatalysts separately on different facets of BiVO₄. *Energy Environ. Sci.* 7, 1369 (2014).

- Ran J., Zhang J., Yu J., and Qiao S.Z.: Enhanced visible-light photocatalytic H₂ production by Zn_xCd_{1-x}S modified with earth-abundant nickel-based cocatalysts. *ChemSusChem* 7, 3426 (2014).
- Young J.L., Steiner M.A., Döscher H., France R.M., Turner J.A., and Deutsch T.G.: Direct solar-to-hydrogen conversion via inverted metamorphic multi-junction semiconductor architectures. *Nat. Energy* 2, 1 (2017).
- Miller E.L.: Photoelectrochemical water splitting. *Energy Environ. Sci.* 8, 2809 (2015).
- Pinaud B.A., Benck J.D., Seitz L.C., Forman A.J., Chen Z., Deutsch T.G., James B.D., Baum K.N., Baum G.N., Ardo S., Wang H., Miller E., and Jaramillo T.F.: Technical and economic feasibility of centralized facilities for solar hydrogen production via photocatalysis and photoelectrochemistry. *Energy Environ. Sci.* 6, 1983 (2013).
- Rashwan S.S., Dincer I., Mohany A., and Pollet B.G.: The Sono-Hydro-Gen process (ultrasound induced hydrogen production): Challenges and opportunities. *Int. J. Hydrogen Energy* 44, 14500 (2019).
- Bhosale R.R., Kumar A., and Sutar P.: Thermodynamic analysis of solar driven SnO₂/SnO based thermochemical water splitting cycle. *Energy Convers. Manage.* 135, 226 (2017).
- Graf D., Monnerie N., Roeb M., Schmitz M., and Sattler C.: Economic comparison of solar hydrogen generation by means of thermochemical cycles and electrolysis. *Int. J. Hydrogen Energy* 33, 4511 (2008).
- Charvin P., Stéphane A., Florent L., and Gilles F.: Analysis of solar chemical processes for hydrogen production from water splitting thermochemical cycles. *Energy Convers. Manage.* 49, 1547 (2008).
- Millet P., Mbemba N., Grigoriev S.A., Fateev V.N., Aukauloo A., and Etiévant C.: Electrochemical performances of PEM water electrolysis cells and perspectives. *Int. J. Hydrogen Energy* 36, 4134 (2011).
- Selamet ÖF, Becerikli F., Mat M.D., and Kaplan Y.: Development and testing of a highly efficient proton exchange membrane (PEM) electrolyzer stack. *Int. J. Hydrogen Energy* 36, 11480 (2011).
- Yin Y., Wang X., Zhang J., Shangguan X., and Qin Y.: Influence of sloping baffle plates on the mass transport and performance of PEMFC. *Int. J. Energy Res.* 43 (2018).
- Carmo M., Fritz D.L., Mergel J., and Stolten D.: A comprehensive review on PEM water electrolysis. *Int. J. Hydrogen Energy* 38, 4901 (2013).
- Grigoriev S.A., Porembsky V.I., and Fateev V.N.: Pure hydrogen production by PEM electrolysis for hydrogen energy. *Int. J. Hydrogen Energy* 31, 171 (2006).
- Phillips R. and Dunnill C.: Zero gap alkaline electrolysis cell design for renewable energy storage as hydrogen gas. *RSC Adv.* 6, 100643 (2016).
- Rashid M., Al Mesfer M., Naseem H., and Danish M.: Hydrogen production by water electrolysis: A review of alkaline water electrolysis, PEM water electrolysis and high temperature water electrolysis. *Int. J. Eng. Adv. Technol.* 4, 2249 (2015).
- Leng Y., Chen G., Mendoza A.J., Tighe T.B., Hickner M.A., and Wang C.-Y.: Solid-state water electrolysis with an alkaline membrane. *J. Am. Chem. Soc.* 134, 9054 (2012).
- Pavel C., Cecconi F., Emiliani C., Santiccioli S., Scaffidi A., Catanorchi S., and Comotti M.: Highly efficient platinum group metal free based membrane-electrode assembly for anion exchange membrane water electrolysis. *Angew. Chem. Int. Ed.* 126, 1378 (2014).
- Moçoteguy P. and Brisse A.: A review and comprehensive analysis of degradation mechanisms of solid oxide electrolysis cells. *Int. J. Hydrogen Energy* 38, 15887 (2013).
- 100. Kadier A., Kalil M.S., Abdeshahian P., Chandrasekhar K., Mohamed A., Azman N.F., Logroño W., Simayi Y., and Hamid A.A.: Recent advances and emerging challenges in microbial electrolysis cells (MECs) for microbial production of hydrogen and value-added chemicals. *Renew. Sustain. Energy Rev.* 61, 501 (2016).
- Zeng K. and Zhang D.: Recent progress in alkaline water electrolysis for hydrogen production and applications. *Prog. Energy Combust. Sci.* 36, 307 (2010).
- Wendt H. and Hofmann H.: Ceramic diaphragms for advanced alkaline water electrolysis. J. Appl. Electrochem. 19, 605 (1989).

- 103. Ayers K.E., Capuano C., and Anderson E.B.: Recent advances in cell cost and efficiency for PEM-based water electrolysis. *ECS Transactions* 41, 15 (2019).
- 104. Bose R., Karuppasamy K., Rajan H., Velusamy D., Kim H.-S., and Alfantazi A.: Electrodeposition of unary oxide on a bimetallic hydroxide as a highly active and stable catalyst for water oxidation. ACS Sustain. Chem. Eng. 7, 16392 (2019).
- 105. Truong L., Jerng S.-K., Roy S.B., Jeon J.H., Kim K., Akbar K., Yi Y., and Chun S.-H.: Chrysanthemum-like CoP nanostructures on vertical graphene nanohills as versatile electrocatalysts for water splitting. *ACS Sustain. Chem. Eng.* 7, 4625 (2019).
- 107. Siracusano S., Van Dijk N., Backhouse R., Merlo L., Baglio V., and Aricò A.S.: Degradation issues of PEM electrolysis MEAs. *Renew. Energy* 123, 52 (2018).
- Frensch S.H., Fouda-Onana F., Serre G., Thoby D., Araya S.S., and Kær S.K.: Influence of the operation mode on PEM water electrolysis degradation. *Int. J. Hydrogen Energy* 44, 29889 (2019).
- 109. Ferriday T. and Middleton P.H.: Experimental analysis of materials in proton exchange membrane electrolysis cells. *Int. J. Hydrogen Energy* 44, 27656 (2019).
- 110. García-Osorio D., Jaimes R., Vazquez-Arenas J., Lara R., and Alvarez-Ramirez J.: The kinetic parameters of the oxygen evolution reaction (OER) calculated on inactive anodes via EIS transfer functions: 'OH formation. J. Electrochem. Soc. 164, E1 (2017).
- 111. Yu J., He Q., Yang G., Zhou W., Shao Z., and Ni M.: Recent advances and prospective in ruthenium-based materials for electrochemical water splitting. ACS Catal. 9, 9973 (2019).
- 112. Wang D., Song Y., Zhang H., Yan X., and Guo J.: Recent advances in transition metal borides for electrocatalytic oxygen evolution reaction. *J. Electroanal. Chem.* 861, 113953 (2020).
- 113. Pareek A., Dom R., Gupta J., Chandran J., Adepu V., and Borse P.H.: Insights into renewable hydrogen energy: Recent advances and prospects. *Mater. Sci. Energy Technol.* 3, 319 (2020).
- 114. Weigt H.: Germany's wind energy: The potential for fossil capacity replacement and cost saving. *Appl. Energy* 86, 1857 (2009).
- 115. Greiner C.J., Korpas M., and Holen A.T.: A Norwegian case study on the production of hydrogen from wind power. *Int. J. Hydrogen Energy* 32, 1500 (2007).
- 116. Ayodele T.R. and Munda J.L.: Potential and economic viability of green hydrogen production by water electrolysis using wind energy resources in South Africa. *Int. J. Hydrogen Energy* 44, 17669 (2019).
- 117. Rezaei M., Naghdi-Khozani N., and Jafari N.: Wind energy utilization for hydrogen production in an underdeveloped country: An economic investigation. *Renew. Energy* 147, 1044 (2020).
- 118. Nadaleti W.C., Borges dos Santos G., and Lourenço V.A.: The potential and economic viability of hydrogen production from the use of hydroelectric and wind farms surplus energy in Brazil: A national and pioneering analysis. *Int. J. Hydrogen Energy* 45, 1373 (2020).
- 119. Jørgensen C. and Ropenus S.: Production price of hydrogen from grid connected electrolysis in a power market with high wind penetration. *Int. J. Hydrogen Energy* 33, 5335 (2008).
- 120. Mueller-Langer F., Tzimas E., Kaltschmitt M., and Peteves S.: Techno-economic assessment of hydrogen production processes for the hydrogen economy for the short and medium term. *Int. J. Hydrogen Energy* 32, 3797 (2007).
- 121. Bazilian M., Onyeji I., Liebreich M., MacGill I., Chase J., Shah J., Gielen D., Arent D., Landfear D., and Zhengrong S.: Re-considering the economics of photovoltaic power. *Renew. Energy* 53, 329 (2013).
- 122. Lagorse J., Simões M.G., Miraoui A., and Costerg P.: Energy cost analysis of a solar-hydrogen hybrid energy system for stand-alone applications. *Int. J. Hydrogen Energy* 33, 2871 (2008).
- 123. Mason J.E. and Zweibel K.: Baseline model of a centralized pv electrolytic hydrogen system. Int. J. Hydrogen Energy 32, 2743 (2007).

- 124. Kikuchi Y., Ichikawa T., Sugiyama M., and Koyama M.: Battery-assisted low-cost hydrogen production from solar energy: Rational target setting for future technology systems. *Int. J. Hydrogen Energy* 44, 1451 (2019).
- 125. Fereidooni M., Mostafaeipour A., Kalantar V., and Goudarzi H.: A comprehensive evaluation of hydrogen production from photovoltaic power station. *Renew. Sust. Energ. Rev.* 82, 415 (2018).
- 126. Al-Sharafi A., Sahin A.Z., Ayar T., and Yilbas B.S.: Techno-economic analysis and optimization of solar and wind energy systems for power generation and hydrogen production in Saudi Arabia. *Renew. Sustain. Energy Rev.* 69, 33 (2017).
- 127. Dufo-López R., Bernal-Agustín J.L., and Mendoza F.: Design and economical analysis of hybrid PV-wind systems connected to the grid for the intermittent production of hydrogen. *Energy Policy* 37, 3082 (2009).
- Dagdougui H., Ouammi A., and Sacile R.: A regional decision support system for onsite renewable hydrogen production from solar and wind energy sources. *Int. J. Hydrogen Energy* 36, 14324 (2011).
- 129. Temiz M. and Javani N.: Design and analysis of a combined floating photovoltaic system for electricity and hydrogen production. *Int. J. Hydrogen Energy* 45, 3457 (2020).
- 130. Olateju B. and Kumar A.: A techno-economic assessment of hydrogen production from hydropower in Western Canada for the upgrading of bitumen from oil sands. *Energy* 115, 604 (2016).
- 131. Yilmaz C., Koyuncu I., Alcin M., and Tuna M.: Artificial neural networks based thermodynamic and economic analysis of a hydrogen production system assisted by geothermal energy on field programmable gate array. *Int. J. Hydrogen Energy* 44, 17443 (2019).
- 132. Hsu C.-H., Chang C.-C., Tseng C.-M., Chan C.-C., Chao W.-H., Wu Y.-R., Wen M.-H., Hsieh Y.-T., Wang Y.-C., and Chen C.-L.: An ultra-fast response gasochromic device for hydrogen gas detection. *Sens. Actuators B* 186, 193 (2013).
- 133. Sherif S.A., Barbir F., and Veziroglu T.N.: Wind energy and the hydrogen economy review of the technology. *Sol. Energy* 78, 647 (2005).
- 134. Louthan M.R.: Hydrogen embrittlement of metals: A primer for the failure analyst. J. Fail. Anal. Prev. 8, 289 (2008).
- 135. Rogers H.C.: Hydrogen embrittlement of metals: Atomic hydrogen from a variety of sources reduces the ductility of many metals. *Science* 159, 1057 (1968).
- 136. Zheng J., Liu X., Xu P., Liu P., Zhao Y., and Yang J.: Development of high pressure gaseous hydrogen storage technologies. *Int. J. Hydrogen Energy* 37, 1048 (2012).
- 137. Alazemi J. and Andrews J.: Automotive hydrogen fuelling stations: An international review. *Renew. Sustain. Energy Rev.* 48, 483 (2015).
- Dagdougui H., Sacile R., Bersani C., and Ouammi A.: Hydrogen Infrastructure for Energy Applications: Production, Storage, Distribution and Safety (Academic Press, Cambridge, MA, USA, 2018).
- 139. Malakhov A.A., Avdeenkov A.V., du Toit M.H., and Bessarabov D.G.: CFD simulation and experimental study of a hydrogen leak in a semi-closed space with the purpose of risk mitigation. *Int. J. Hydrogen Energy* 45, 9231 (2020).
- 140. Mazloomi K. and Gomes C.: Hydrogen as an energy carrier: Prospects and challenges. *Renew. Sustain. Energy Rev.* 16, 3024 (2012).
- 141. Villalonga S., Nony F., Magnier C., Yvernes J., Thomas C., Delmas B., and Mazabraud P.: Composite 700 bar-vessel for on-board compressed gaseous hydrogen storage. In *Proceeding of 17th International Conference on Composite Materials*, Edinburgh, UK (2009).
- 142. Züttel A.: Hydrogen storage methods. Naturwissenschaften 91, 157 (2004).
- 143. Bossel U.: Does a hydrogen economy make sense? In Proceedings of the IEEE (2006), p. 1826.
- 144. Zhou L.: Progress and problems in hydrogen storage methods. *Renew. Sustain Energy Rev.* 9, 395 (2005).
- 145. Züttel A.: Materials for hydrogen storage. Mater. Today 6, 24 (2003).
- 146. Li Y., Chen H., Zhang X., Tan C., and Ding Y.: Renewable energy carriers: Hydrogen or liquid air/nitrogen? *Appl. Therm. Eng.* 30, 1985 (2010).
- 147. Schlapbach L. and Zuttel A.: Hydrogen-storage materials for mobile applications. *Nature* 414, 353 (2001).
- 148. Nijkamp M., Raaymakers J., Van Dillen A., and De Jong K.: Hydrogen storage using physisorption-materials demands. *Appl. Phys. A* 72, 619 (2001).

- Blankenship T.S. II, Balahmar N., and Mokaya R.: Oxygen-rich microporous carbons with exceptional hydrogen storage capacity. *Nat. Commun.* 8, 1 (2017).
- 150. Zhou L., Liu D., Li J., Tang H., Xie Z., and Qu D.: Electrochemical hydrogen storage in a nitrogen-doped uniformed microporous carbon. *Int. J. Hydrogen Energy* 43, 14096 (2018).
- 151. Li Y., Liu H., Yang C., Zhu M., and Chen T.: The activation and hydrogen storage characteristics of the cup-stacked carbon nanotubes. *Diamond Relat. Mater.* 100, 107567 (2019).
- 152. Mohan M., Sharma V.K., Kumar E.A., and Gayathri V.: Hydrogen storage in carbon materials-A review. *Energy Storage* 1, E35 (2019).
- Weitkamp J., Fritz M., and Ernst S.: Zeolites as media for hydrogen storage. Int. J. Hydrogen Energy 20, 967 (1995).
- 154. Yang Z., Xia Y., and Mokaya R.: Enhanced hydrogen storage capacity of high surface area zeolite-like carbon materials. *J. Am. Chem. Soc.* 129, 1673 (2007).
- 155. Molefe L.Y., Musyoka N.M., Ren J., Langmi H.W., Mathe M., and Ndungu P.G.: Polymer-based shaping strategy for zeolite templated carbon (ZTC) and their metal organic framework (MOF) composites for improved hydrogen storage properties. *Front. Chem.* 7, 864 (2019).
- 156. Ismail N. and Tantawy H.A.: Microwave synthesis of nano/micronized zeolites from natural source: Evaluation of energy storage capacities. *Egypt. J. Chem.* 63, 8 (2020).
- 157. Bose R., Ethiraj J., Sridhar P., Varghese J.J., Kaisare N.S., and Selvam P.: Adsorption of hydrogen and carbon dioxide in zeolitic imidazolate framework structure with SOD topology: Experimental and modelling studies. *Adsorption* 1 (2020).
- 158. Xu J., Liu J., Li Z., Wang X., Xu Y., Chen S., and Wang Z.: Optimized synthesis of Zr (IV) metal organic frameworks (MOFs-808) for efficient hydrogen storage. *New J. Chem.* 43, 4092 (2019).
- 159. Suh M.P., Park H.J., Prasad T.K., and Lim D.W.: Hydrogen storage in metal-organic frameworks. *Chem. Rev.* 112, 782 (2012).
- Murray L.J., Dinca M., and Long J.R.: Hydrogen storage in metal-organic frameworks. *Chem. Soc. Rev.* 38, 1294 (2009).
- Rowsell J.L.C. and Yaghi O.M.: Strategies for hydrogen storage in metal-organic frameworks. *Angew. Chem. Int. Ed.* 44, 4670 (2005).
- 162. Gangu K.K., Maddila S., Mukkamala S.B., and Jonnalagadda S.B.: Characteristics of MOF, MWCNT and graphene containing materials for hydrogen storage: A review J. Energy Chem. 30, 132 (2019).
- 163. Bobbitt N.S. and Snurr R.Q.: Molecular modelling and machine learning for high-throughput screening of metal-organic frameworks for hydrogen storage. *Mol. Simulat.* 45, 1069 (2019).
- 164. Lim K.L., Kazemian H., Yaakob Z., and Daud W.R.W.: Solid-state materials and methods for hydrogen storage: A critical review. *Chem. Eng. Technol.* 33, 213 (2010).
- Ramimoghadam D., Gray E.M., and Webb C.J.: Review of polymers of intrinsic microporosity for hydrogen storage applications. *Int. J. Hydrogen Energy* 41, 16944 (2016).
- 166. Lai Q., Sun Y., Wang T., Modi P., Cazorla C., Demirci U.B., Ares Fernandez J.R., Leardini F., and Aguey-Zinsou K.F.: How to design hydrogen storage materials? Fundamentals, synthesis, and storage tanks. *Adv. Sustain. Syst.* 3, 1900043 (2019).
- 167. Zhang F., Zhao P., Niu M., and Maddy J.: The survey of key technologies in hydrogen energy storage. *Int. J. Hydrogen Energy* 41, 14535 (2016).
- 168. Sujan G., Pan Z., Li H., Liang D., and Alam N.: An overview on TiFe intermetallic for solid-state hydrogen storage: Microstructure, hydrogenation and fabrication processes. *Crit. Rev. Solid State Mater. Sci.* 1, 1 (2019).
- 169. Kumar S., Kojima Y., and Dey G.K.: Thermodynamics and kinetics of hydrogen absorption-desorption of highly crystalline LaNi₅. J. Therm. Anal. Calorim. 134, 889 (2018).
- Broom D.P.: Hydrogen Storage Materials: The Characterisation of Their Storage Properties (Springer Science & Business Media, Berlin, Germany, 2011).
- 171. Dalebrook A.F., Gan W., Grasemann M., Moret S., and Laurenczy G.: Hydrogen storage: Beyond conventional methods. *Chem. Commun.* 49, 8735 (2013).

- 172. Wang T. and Aguey-Zinsou K.F.: Controlling the growth of $LiBH_4$ nanoparticles for hydrogen storage. *Energy Technol.* 7, 1801159 (2019).
- 173. Benzidi H., Lakhal M., Abdellaoui M., Garara M., Benyoussef A., Loulidi M., Hamedoun M., and Mounkachi O.: Improved thermodynamic properties of doped LiBH₄ for hydrogen storage: First-principal calculation. *Int. J. Hydrogen Energy* 44, 16793 (2019).
- 174. Sinigaglia T., Lewiski F., Martins M.E.S., and Siluk J.C.M.: Production, storage, fuel stations of hydrogen and its utilization in automotive applications - a review. *Int. J. Hydrogen Energy* 42, 24597 (2017).
- 175. Li X.J., Allen J.D., Stager J.A., and Ku A.Y.: Paths to low-cost hydrogen energy at a scale for transportation applications in the USA and China via liquid-hydrogen distribution networks. *Clean Energy* 4, 26 (2020).
- 176. Wiser R., Jenni K., Seel J., Baker E., Hand M., Lantz E., and Smith A.: Expert elicitation survey on future wind energy costs. *Nat. Energy* 1, 1 (2016).
- 177. Comello S., Reichelstein S., and Sahoo A.: The road ahead for solar PV power. *Renew. Sustain. Energy Rev.* 92, 744 (2018).
- Felgenhauer M. and Hamacher T.: State-of-the-art of commercial electrolyzers and on-site hydrogen generation for logistic vehicles in South Carolina. *Int. J. Hydrogen Energy* 40, 2084 (2015).
- Glenk G. and Reichelstein S.: Economics of converting renewable power to hydrogen. *Nat. Energy* 4, 216 (2019).
- National Research Council: *The Hydrogen Economy: Opportunities, Costs, Barriers, and R&D Needs* (National Academies Press, Washington, D.C., USA, 2004).

- 181. Garcia D.A.: Analysis of non-economic barriers for the deployment of hydrogen technologies and infrastructures in European countries. *Int. J. Hydrogen Energy* 42, 6435 (2017).
- 182. Dolci F., Thomas D., Hilliard S., Guerra C.F., Hancke R., Ito H., Jegoux M., Kreeft G., Leaver J., Newborough M., Proost J., Robinius M., Weidner E., Mansilla C., and Lucchese P.: Incentives and legal barriers for power-to-hydrogen pathways: An international snapshot. *Int. J. Hydrogen Energy* 44, 11394 (2019).
- 183. Rogelj J., Den Elzen M., Höhne N., Fransen T., Fekete H., Winkler H., Schaeffer R., Sha F., Riahi K., and Meinshausen M.: Paris Agreement climate proposals need a boost to keep warming well below 2°C. *Nature* 534, 631 (2016).
- 184. Kosturjak A., Dey T., Young M.D., and Whetton S.: Advancing Hydrogen: Learning From 19 Plans to Advance Hydrogen From Across the Globe (Future Fuels CRC, 2019), Australia.
- Mohsin M., Rasheed A., and Saidur R.: Economic viability and production capacity of wind generated renewable hydrogen. *Int. J. Hydrogen Energy* 43, 2621 (2018).
- 186. Hydrogen From Renewable Power: Technology Outlook for the energy transition, (IRENA, International Renewable Energy Agency, 2018), Abu Dhabi.
- 187. Abad A.V. and Dodds P.E.: Green hydrogen characterisation initiatives: Definitions, standards, guarantees of origin, and challenges. *Energy Policy* 138, 111300 (2020).